

Input file: H:\dos\Conferences&Publications\Paper for Building and environment\C32\_@\_1C.pqi

Output file: H:\dos\Conferences&Publications\Paper for Building and environment\C32\_@\_1C.pqi

Database file: C:\Program Files\USGS\Phreeqc Interactive 3.1.7-9213\database\llnl.dat

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Reading data base.  
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LLNL\_AQUEOUS\_MODEL\_PARAMETERS  
NAMED\_EXPRESSIONS  
SOLUTION\_MASTER\_SPECIES  
SOLUTION\_SPECIES  
PHASES  
EXCHANGE\_MASTER\_SPECIES  
EXCHANGE\_SPECIES  
SURFACE\_MASTER\_SPECIES  
SURFACE\_SPECIES  
RATES  
END

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Reading input data for simulation 1.  
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DATABASE C:\Program Files\USGS\Phreeqc Interactive 3.1.7-9213\database\llnl.dat  
SOLUTION 1  
temp 25  
pH 7 charge  
pe 4  
redox pe  
units mol/kgw  
density 1  
Alkalinity 0  
water 1 # kg  
EQUILIBRIUM\_PHASES 1  
Calcite 0 1000  
Portlandite 0 1000  
CO2(g) -3.408822658 100  
NO2(g) -5.149185348 100  
END

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Beginning of initial solution calculations.  
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Initial solution 1.

-----Solution composition-----

Elements	Molality	Moles
Pure water		

-----Description of solution-----

pH	=	7.008	Charge balance
pe	=	4.000	
Activity of water	=	1.000	
Ionic strength	=	9.819e-08	
Mass of water (kg)	=	1.000e+00	
Total alkalinity (eq/kg)	=	1.060e-17	
Total carbon (mol/kg)	=	0.000e+00	
Total CO2 (mol/kg)	=	0.000e+00	
Temperature (°C)	=	25.00	
Electrical balance (eq)	=	-1.060e-17	
Percent error, 100*(Cat- An )/(Cat+ An )	=	-0.00	

Iterations = 2  
Total H = 1.110507e+02  
Total O = 5.552533e+01

-----Distribution of species-----

Species	Molality	Activity	Log Molality	Log Activity	Log Gamma	mole V cm <sup>3</sup> /mol
OH-	9.819e-08	9.816e-08	-7.008	-7.008	-0.000	(0)
H+	9.819e-08	9.816e-08	-7.008	-7.008	-0.000	0.00
H2O	5.553e+01	1.000e+00	1.744	-0.000	0.000	18.07
H(0)	1.529e-25					
H2	7.645e-26	7.645e-26	-25.117	-25.117	0.000	(0)
O(0)	0.000e+00					
O2	0.000e+00	0.000e+00	-41.963	-41.963	0.000	(0)

-----Saturation indices-----

Phase	SI**	log IAP	log K(298 K, 1 atm)	
H2(g)	-22.02	-25.12	-3.10	H2
H2O(g)	-1.59	-0.00	1.59	H2O
Ice	-0.14	-0.00	0.14	H2O
O2(g)	-39.07	-41.96	-2.89	O2

\*\*For a gas, SI = log10(fugacity). Fugacity = pressure \* phi / 1 atm.  
For ideal gases, phi = 1.

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Beginning of batch-reaction calculations.  
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Reaction step 1.

WARNING: Maximum iterations exceeded, 100

WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying smaller step size, pe step size 10, 5 ...

WARNING: Mass of water is less than 1e-10 kilogram.  
The aqueous phase may not be stable relative to given masses of minerals.  
WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying reduced tolerance 1e-16 ...

WARNING: Mass of water is less than 1e-10 kilogram.  
The aqueous phase may not be stable relative to given masses of minerals.  
WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying increased tolerance 1e-14 ...

WARNING: Mass of water is less than 1e-10 kilogram.  
The aqueous phase may not be stable relative to given masses of minerals.  
WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying diagonal scaling ...

WARNING: Mass of water is less than 1e-10 kilogram.  
The aqueous phase may not be stable relative to given masses of minerals.  
WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying diagonal scaling and reduced tolerance 1e-16 ...

WARNING: Maximum iterations exceeded, 200

WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying scaling pure\_phase columns 1e-10 ...

WARNING: Maximum iterations exceeded, 200

WARNING: Numerical method failed with this set of convergence parameters.

WARNING: Trying scaling pure\_phase columns and diagonal scale 1e-10 ...

Using solution 1.

Using pure phase assemblage 1.

-----Phase assemblage-----

Phase	SI	log IAP	log K(T, P)	Moles in assemblage		
				Initial	Final	Delta
CO2(g)	-13.15	-20.98	-7.83	1.000e+02	0	-1.000e+02
Calcite	0.00	1.82	1.82	1.000e+03	1.100e+03	1.000e+02
NO2(g)	-15.97	-7.62	8.35	1.000e+02	0	-1.000e+02
Portlandite	0.00	22.55	22.55	1.000e+03	8.600e+02	-1.400e+02

-----Solution composition-----

Elements	Molality	Moles
C	6.928e-06	2.440e-05
Ca	1.136e+01	4.002e+01
N	2.840e+01	1.000e+02

-----Description of solution-----

pH = 11.858                    Charge balance  
 pe = 6.846                     Adjusted to redox equilibrium  
 Activity of water = 0.556  
 Ionic strength = 1.246e+01  
 Mass of water (kg) = 3.521e+00  
 Total alkalinity (eq/kg) = 1.072e-02  
 Total CO2 (mol/kg) = 6.928e-06  
 Temperature (°C) = 25.00  
 Electrical balance (eq) = -4.449e-11  
 Percent error, 100\*(Cat-|An|)/(Cat+|An|) = -0.00  
 Iterations = 33  
 Total H = 3.910884e+02  
 Total O = 4.355631e+02

-----Distribution of species-----

Species	Molality	Activity	Log Molality	Log Activity	Log Gamma	mole V cm <sup>3</sup> /mol
OH-	2.708e-03	3.861e-03	-2.567	-2.413	0.154	(0)
H+	6.155e-13	1.387e-12	-12.211	-11.858	0.353	0.00
H2O	5.553e+01	5.561e-01	1.744	-0.255	0.000	18.07
C(-2)	0.000e+00					
C2H4	0.000e+00	0.000e+00	-261.812	-261.812	0.000	(0)
C(-3)	0.000e+00					
C2H6	0.000e+00	0.000e+00	-230.333	-230.333	0.000	(0)
C(-4)	0.000e+00					
CH4	0.000e+00	0.000e+00	-142.199	-142.199	0.000	(0)
C(2)	0.000e+00					
CO	0.000e+00	0.000e+00	-56.806	-56.806	0.000	(0)
C(4)	6.928e-06					
CaCO3	6.867e-06	6.867e-06	-5.163	-5.163	0.000	(0)

CO3-2	6.032e-08	1.352e-08	-7.220	-7.869	-0.650	(0)
CaHCO3+	7.077e-10	1.098e-09	-9.150	-8.959	0.191	(0)
HCO3-	2.724e-10	4.227e-10	-9.565	-9.374	0.191	(0)
CO2	1.756e-16	2.446e-15	-15.755	-14.612	1.144	(0)
Ca	1.136e+01					
CaNO3+	1.081e+01	1.677e+01	1.034	1.225	0.191	(0)
Ca+2	5.456e-01	2.192e-01	-0.263	-0.659	-0.396	(0)
CaOH+	7.999e-03	1.241e-02	-2.097	-1.906	0.191	(0)
CaCO3	6.867e-06	6.867e-06	-5.163	-5.163	0.000	(0)
CaHCO3+	7.077e-10	1.098e-09	-9.150	-8.959	0.191	(0)
H(0)	0.000e+00					
H2	0.000e+00	0.000e+00	-41.652	-40.508	1.144	(0)
N(-03)	0.000e+00					
N3-	0.000e+00	0.000e+00	-62.600	-62.409	0.191	(0)
HN3	0.000e+00	0.000e+00	-69.564	-69.564	0.000	(0)
N(-3)	0.000e+00					
NH3	0.000e+00	0.000e+00	-49.618	-49.618	0.000	(0)
NH4+	0.000e+00	0.000e+00	-52.284	-52.236	0.048	(0)
N(0)	5.680e+00					
N2	2.840e+00	2.840e+00	0.453	0.453	0.000	(0)
N(3)	4.871e-09					
NO2-	4.871e-09	6.245e-09	-8.312	-8.204	0.108	(0)
HNO2	1.479e-17	1.479e-17	-16.830	-16.830	0.000	(0)
N(5)	2.272e+01					
NO3-	1.191e+01	1.527e+01	1.076	1.184	0.108	(0)
CaNO3+	1.081e+01	1.677e+01	1.034	1.225	0.191	(0)
HNO3	1.108e-12	1.108e-12	-11.956	-11.956	0.000	(0)
O(0)	2.935e-13					
O2	1.467e-13	2.044e-12	-12.833	-11.690	1.144	(0)

-----Saturation indices-----

Phase	SI**	log IAP	log K(298 K,	1 atm)	
Aragonite	-0.15	1.82	1.97	CaCO3	
C	-73.43	-9.29	64.15	C	
C(g)	-191.05	-9.29	181.77	C	
Ca	-111.19	28.65	139.83	Ca	
Ca(g)	-136.43	28.65	165.07	Ca	
Calcite	0.00	1.82	1.82	CaCO3	
CH4(g)	-139.36	-142.20	-2.84	CH4	
CO(g)	-53.81	-56.81	-3.00	CO	
CO2(g)	-13.15	-20.98	-7.83	CO2	
H2(g)	-37.41	-40.51	-3.10	H2	
H2O(g)	-1.84	-0.25	1.59	H2O	
Ice	-0.39	-0.25	0.14	H2O	
Lime	-9.77	22.80	32.57	CaO	
Monohydrocalcite	-1.11	1.57	2.68	CaCO3:H2O	
N2(g)	3.63	0.45	-3.18	N2	
NH3(g)	-51.41	-49.62	1.80	NH3	
NO(g)	-17.75	-17.01	0.74	NO	
NO2(g)	-15.97	-7.62	8.35	NO2	
O2(g)	-8.80	-11.69	-2.89	O2	
Portlandite	0.00	22.55	22.55	Ca(OH)2	

\*\*For a gas, SI = log10(fugacity). Fugacity = pressure \* phi / 1 atm.  
For ideal gases, phi = 1.

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End of simulation.  
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Reading input data for simulation 2.  
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End of Run after 0.47 Seconds.  
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